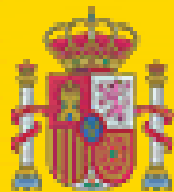


MEDITERRANEAN WORKSHOP ON  
NEW TECHNOLOGIES OF RECYCLING NON  
CONVENTIONAL WATER IN PROTECTED CULTIVATION  
AGADIR (29 April-1 May, 2008)

**SOLAR DESALINATION – RECENT**  
**RESEARCH ACTIVITIES OF**  
**PLATAFORMA SOLAR DE ALMERIA**

**Dr. Sixto Malato**  
**Plataforma Solar de Almeria**  
**Sixto.malato@psa.es**

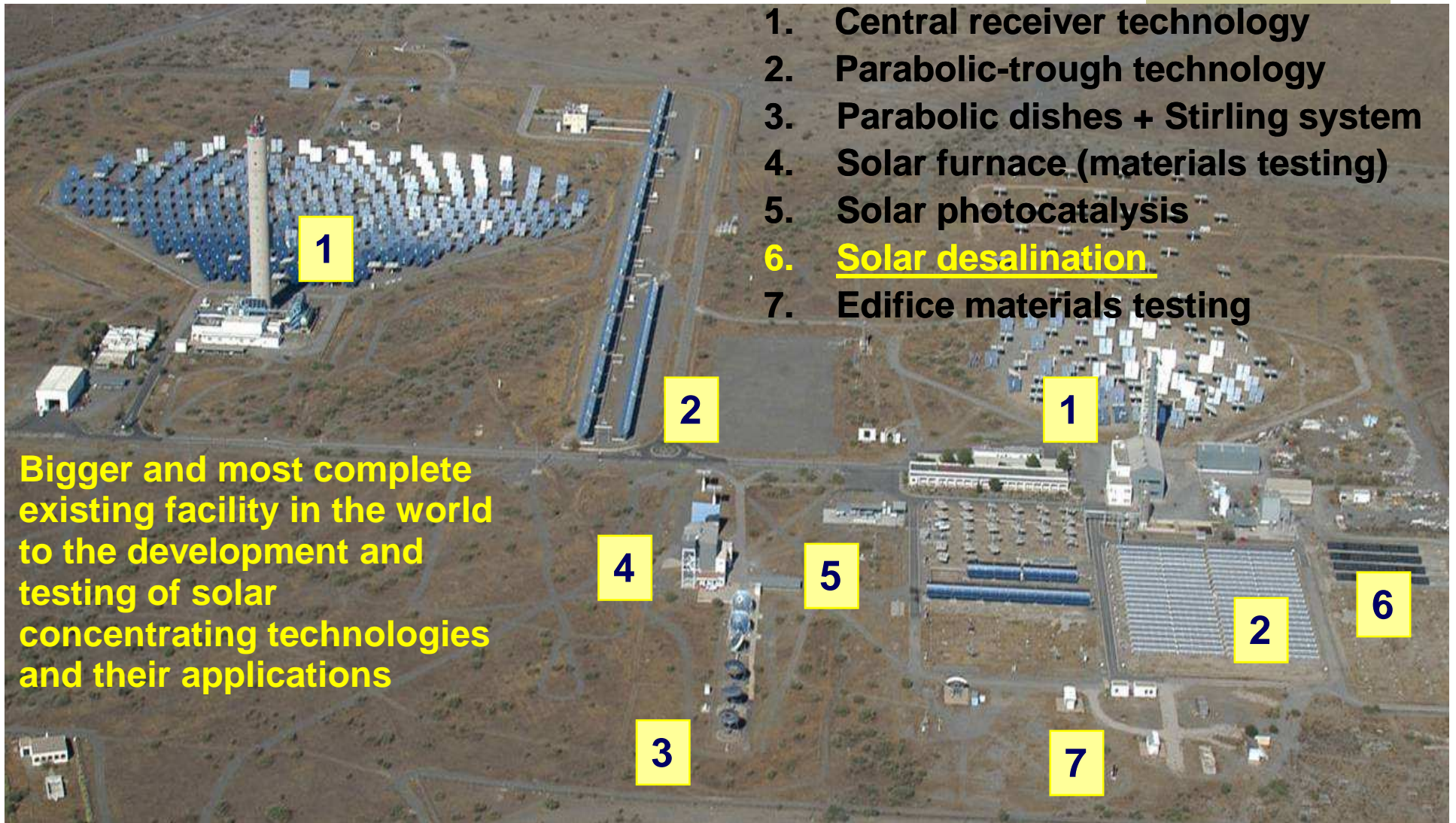


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# PLATAFORMA SOLAR DE ALMERÍA



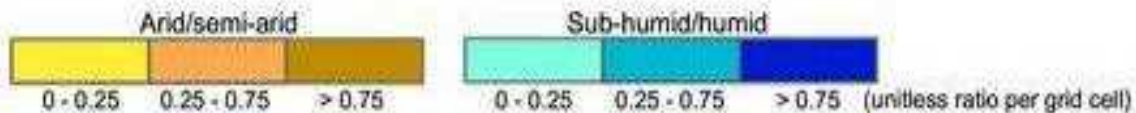
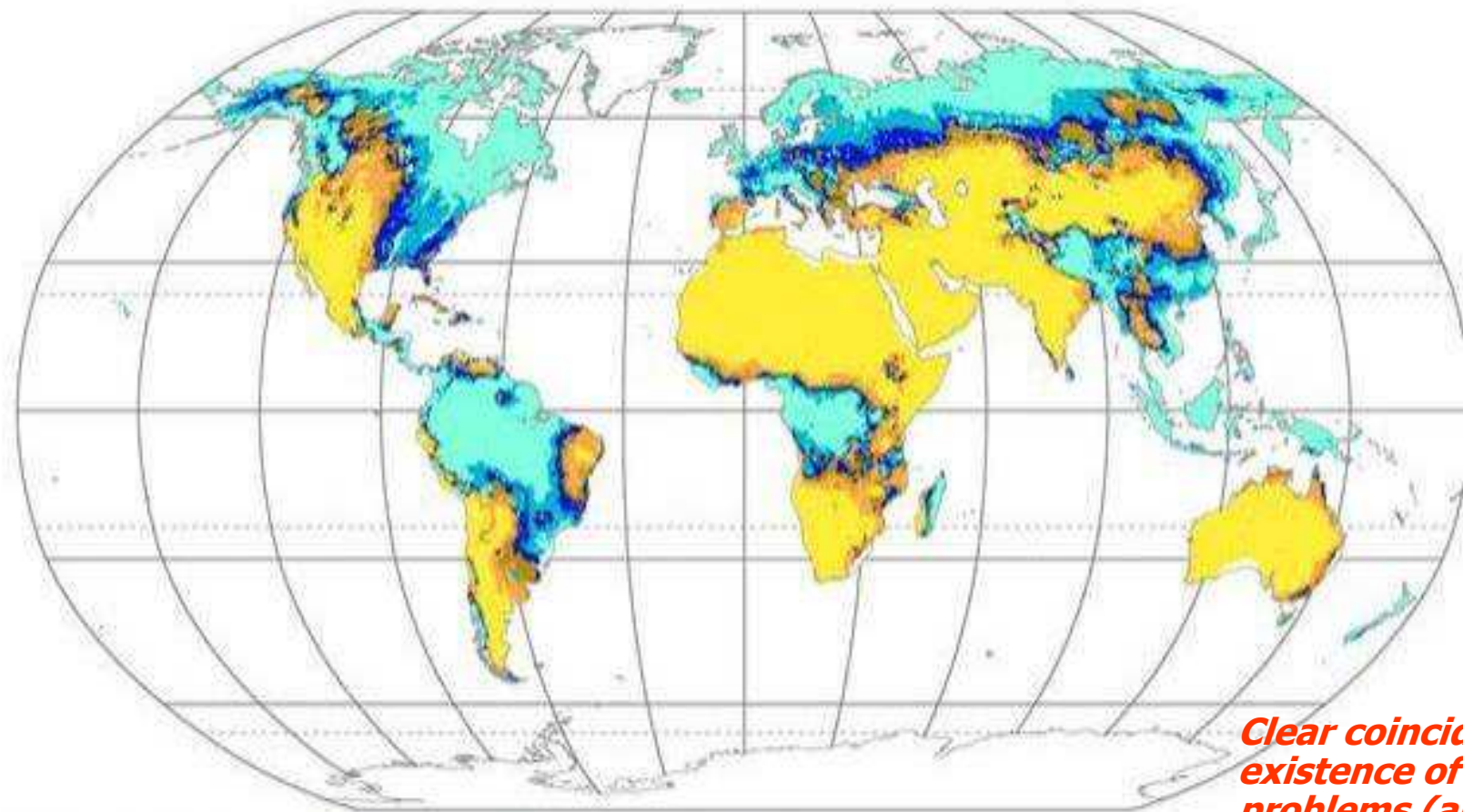


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# SOLAR ENERGY & ARID ZONES



*Clear coincidence in the existence of water problems (arid and semi-arid zones) and the availability of abundant solar radiation*

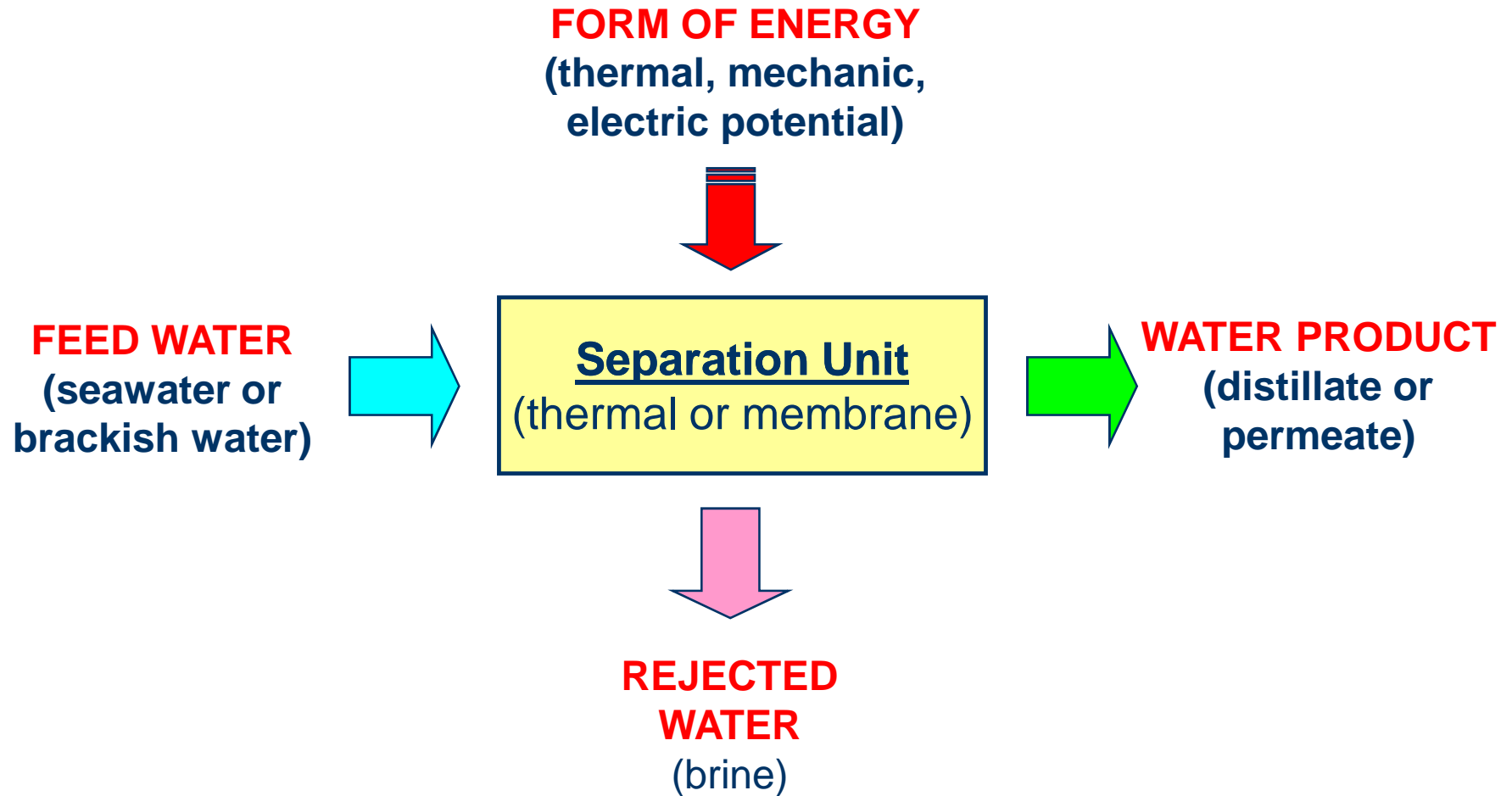


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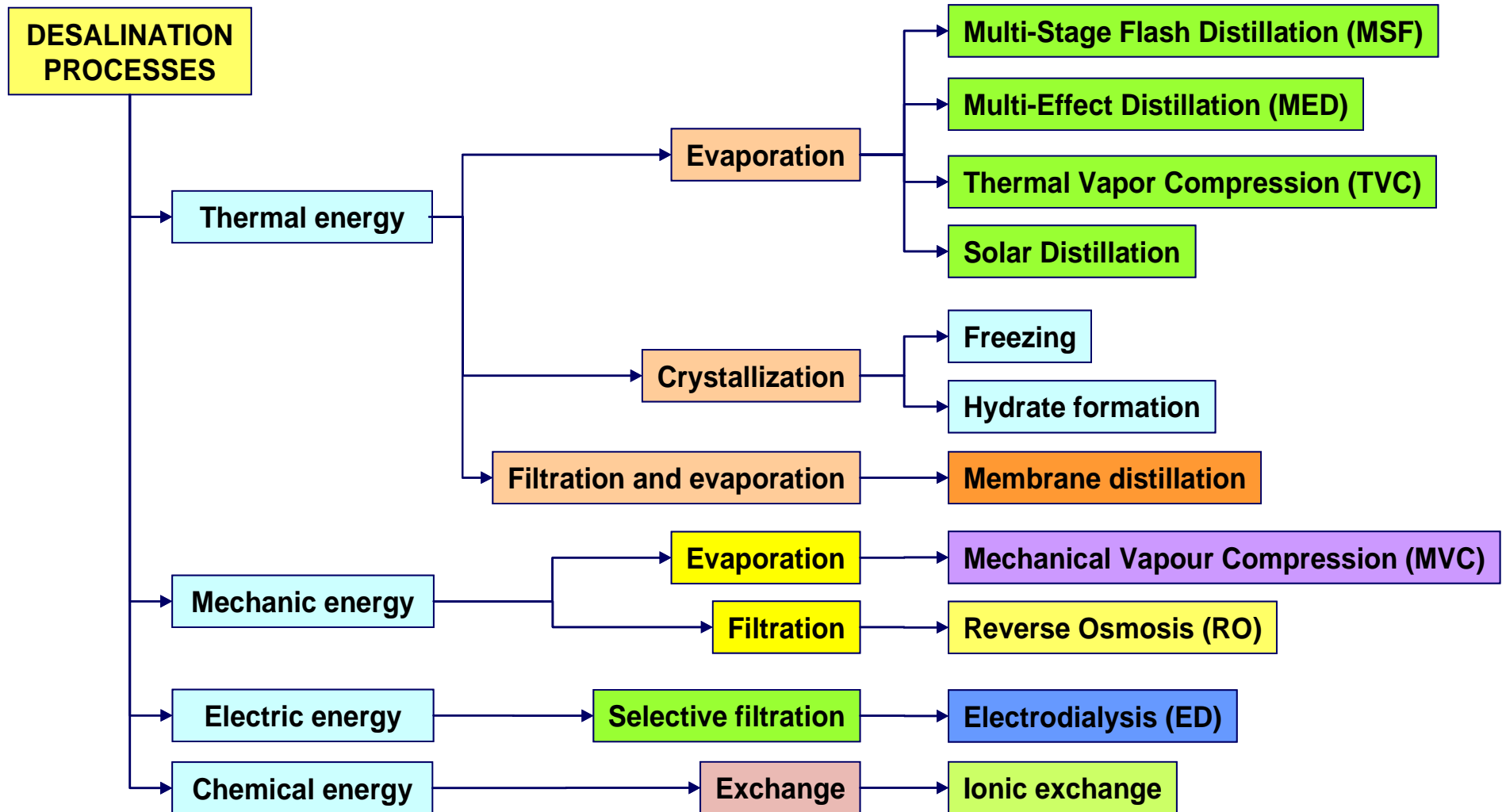


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# THE DESALINATION PROCESS

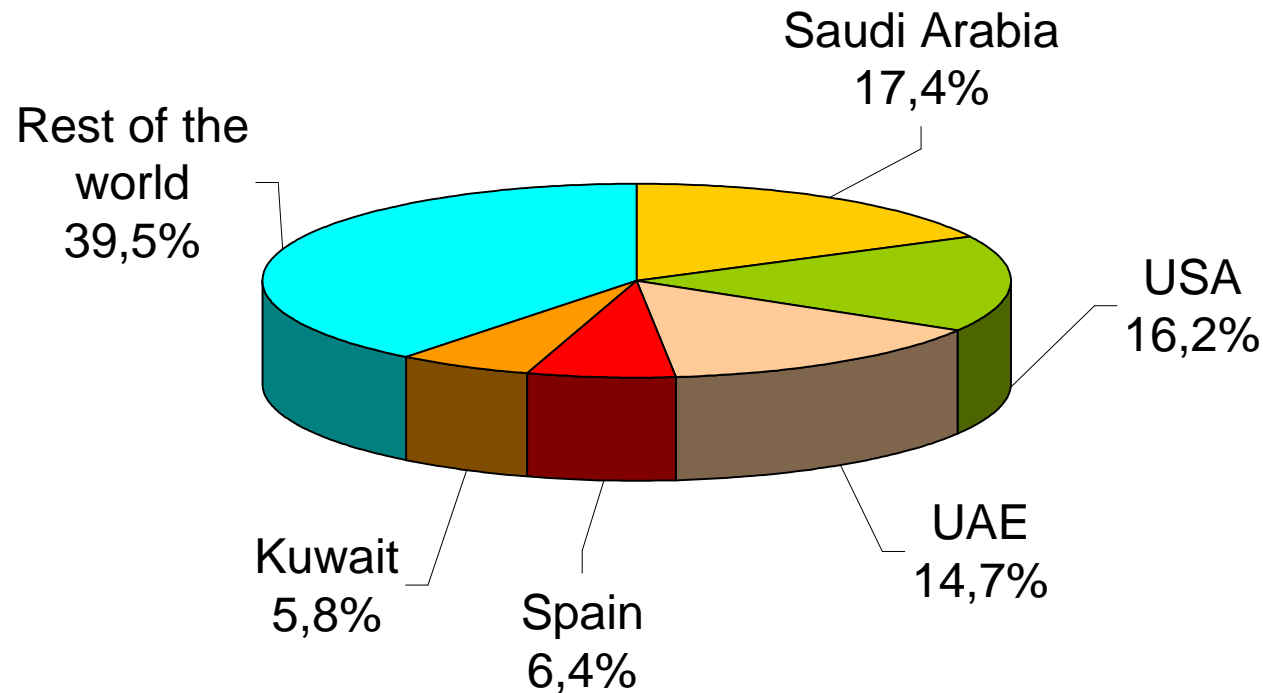


# DESALINATION PROCESSES



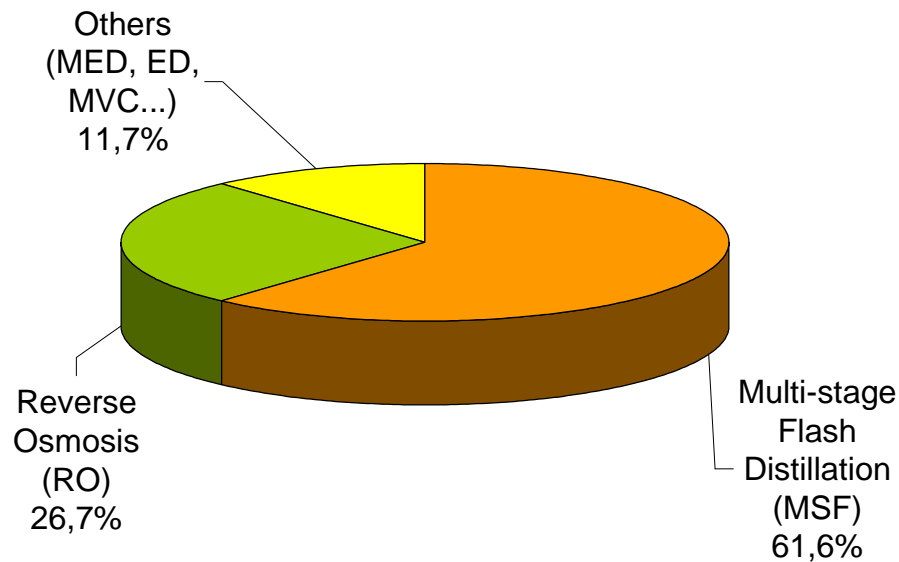
# WORLD CAPACITY DISTRIBUTION

Five countries (Saudi Arabia, USA, UAE, Spain and Kuwait) share more than 60% of the world production capacity of desalinated water.

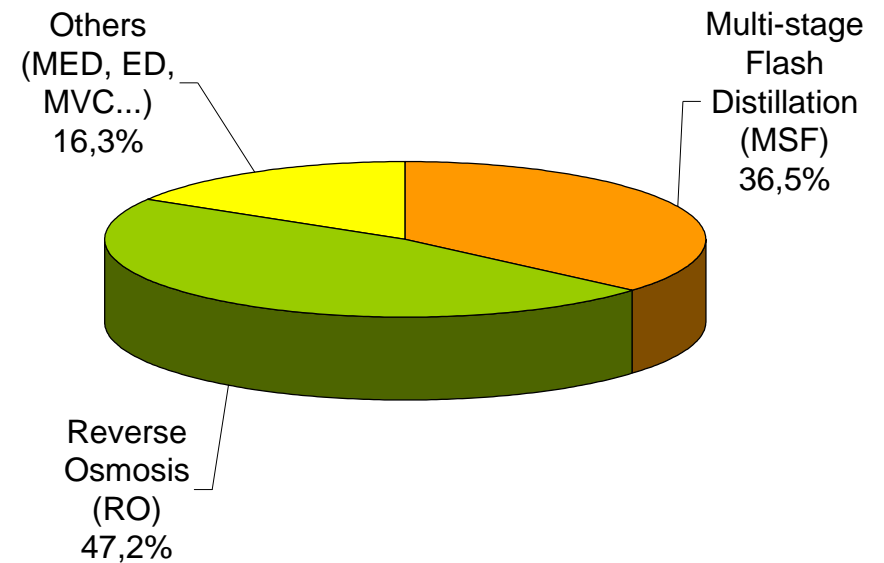


# PROCESS DISTRIBUTION CAPACITY

## Sea water

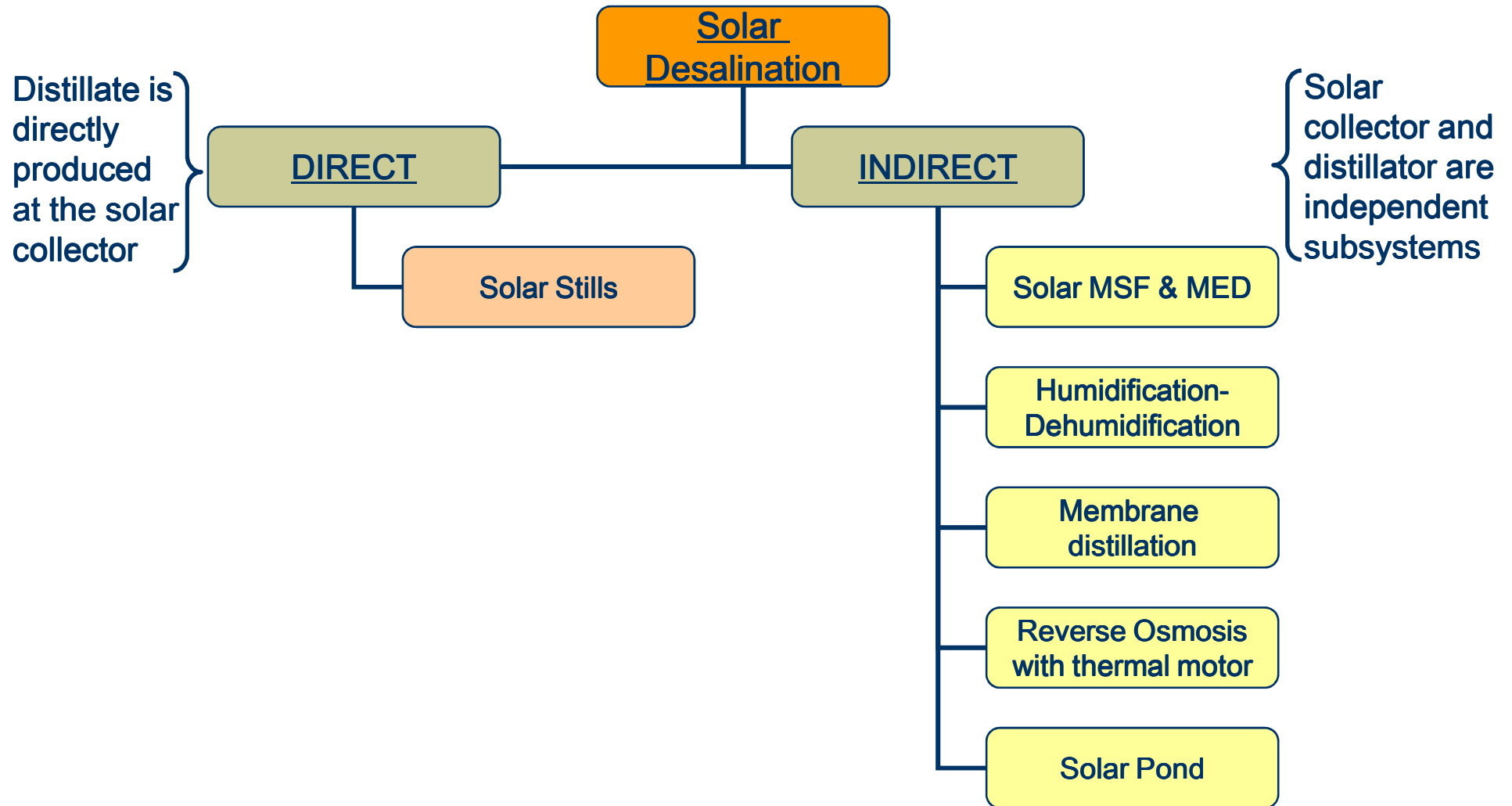


## Sea water + brackish water





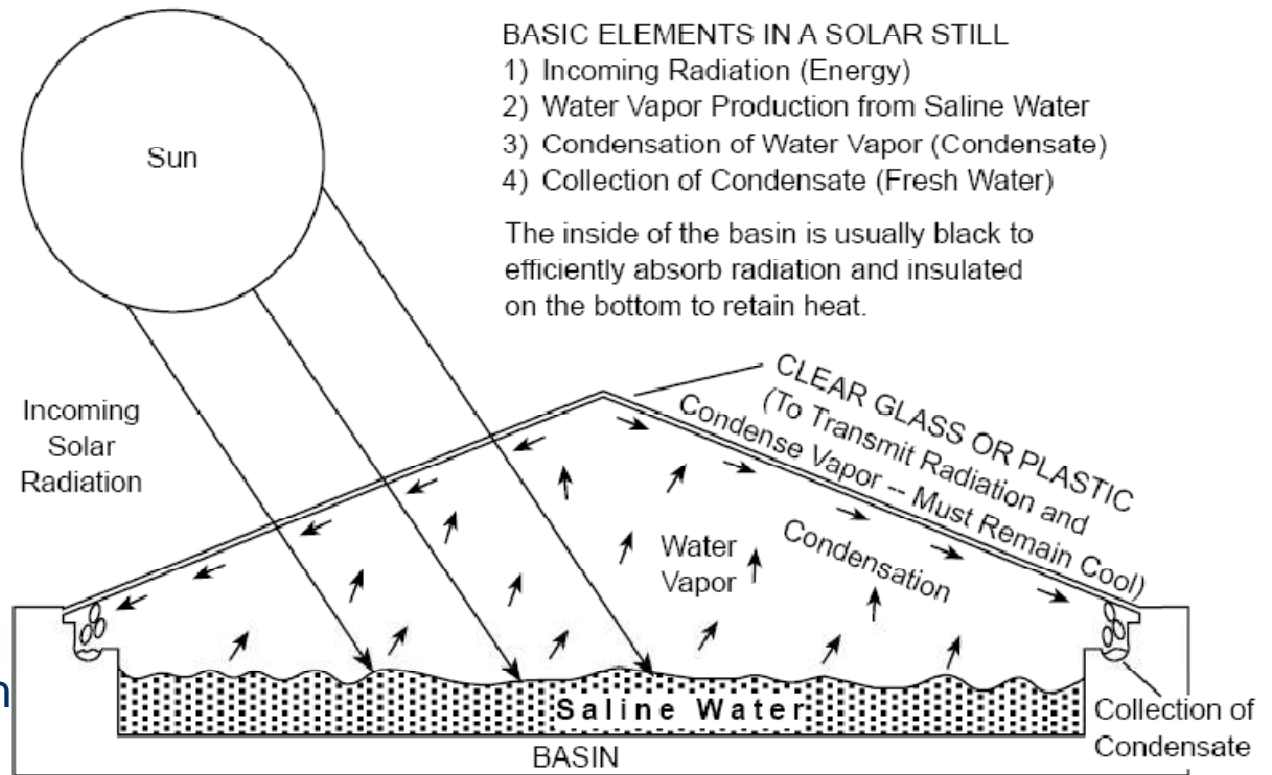
# SOLAR THERMAL DESALINATION



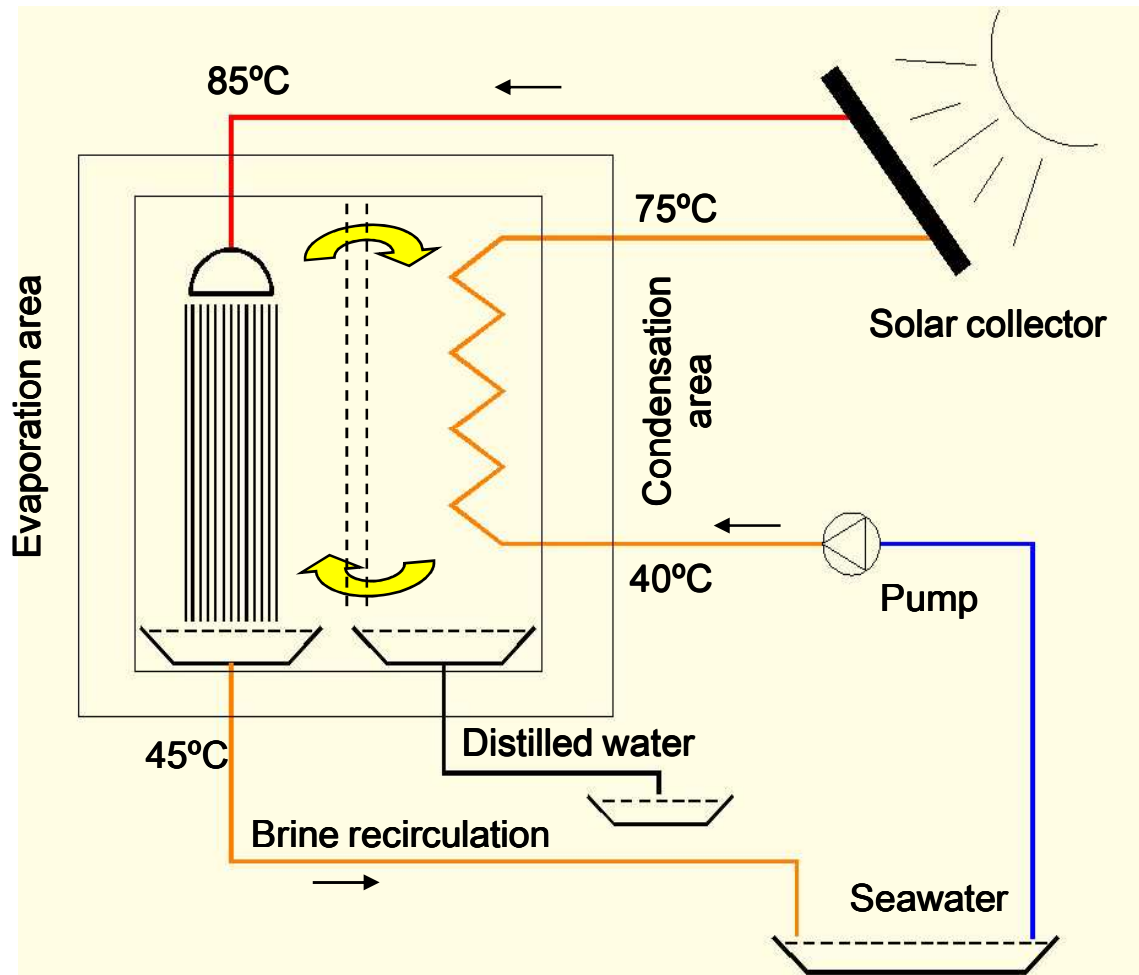
# SOLAR STILLS

**Parameters that affect efficiency** of solar stills include water depth, solar radiation intensity, cover inclination and material, and feed water temperature.

Solar Still present a low distillate production per surface unit (between **1 and 4 L/m<sup>2</sup>/d**). Typical **Performance Ratio** of a solar still is about **0.53**, which means that **4652 kJ** are required to produce one kilogram of desalted water.



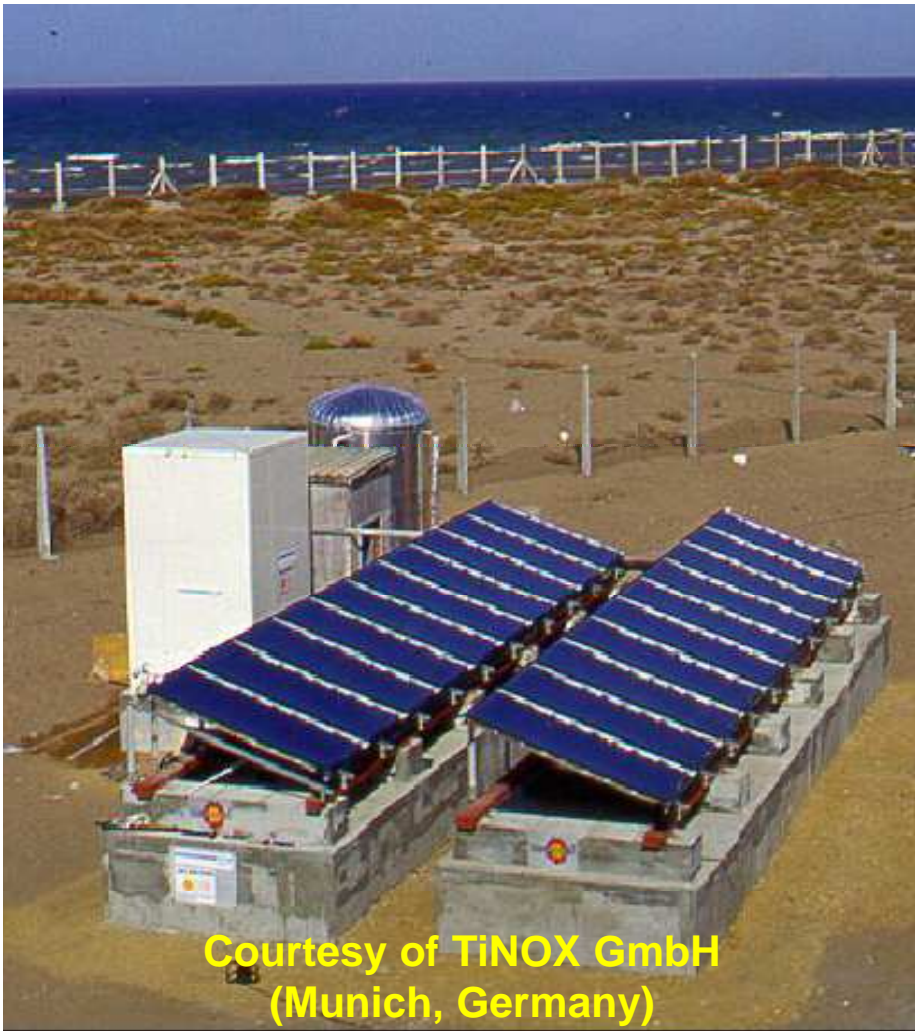
# HUMIDIFICATION-DEHUMIDIFICATION



Desalination process based on the increase of water saturation capacity of air with temperature. Thermal energy can be provided by flat solar collectors. Typical distillate production: **10 to 20 L/m<sup>2</sup>** (of solar collector) **and day**



# HUMIDIFICATION-DEHUMIDIFICATION



Courtesy of TiNOX GmbH  
(Munich, Germany)

**TiNOX GmbH (Germany)** is currently manufacturing 3 systems based on the multi-effect humidification-dehumidification process with nominal production of: 1000, 5000 and 10000 L/day.



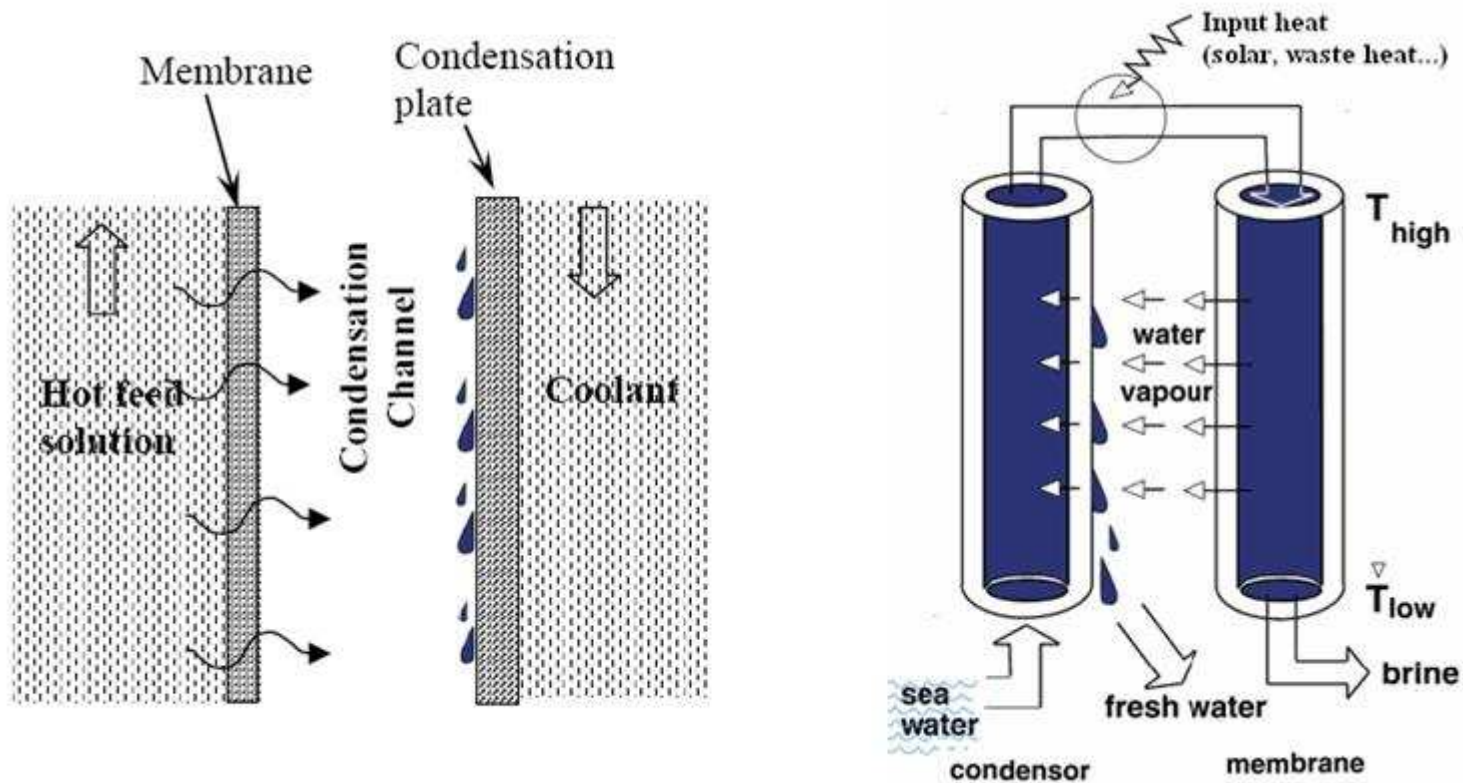
TiNOX GmbH

5000 L/day system installed on Jeddah, (Saudi Arabia) with 140 m<sup>2</sup> of solar collectors and a 10 m<sup>3</sup> thermal storage tank at 90°C



# MEMBRANE DISTILLATION

Distillation driven by partial pressure difference on the two sides of a hydrophobic membrane which permit the flow of vapor but not the liquid water



# MEMBRANE DISTILLATION

The Fraunhofer Institut (Germany) is working on the development of two systems based on this process: **100 L/day** (1 membrane, 6 m<sup>2</sup> of solar collectors) and **1000 L/day** (4 membranes, 72 m<sup>2</sup> of solar collectors). Typical distillate production: **15 to 20 L/m<sup>2</sup>** (of solar collector) **and day**.



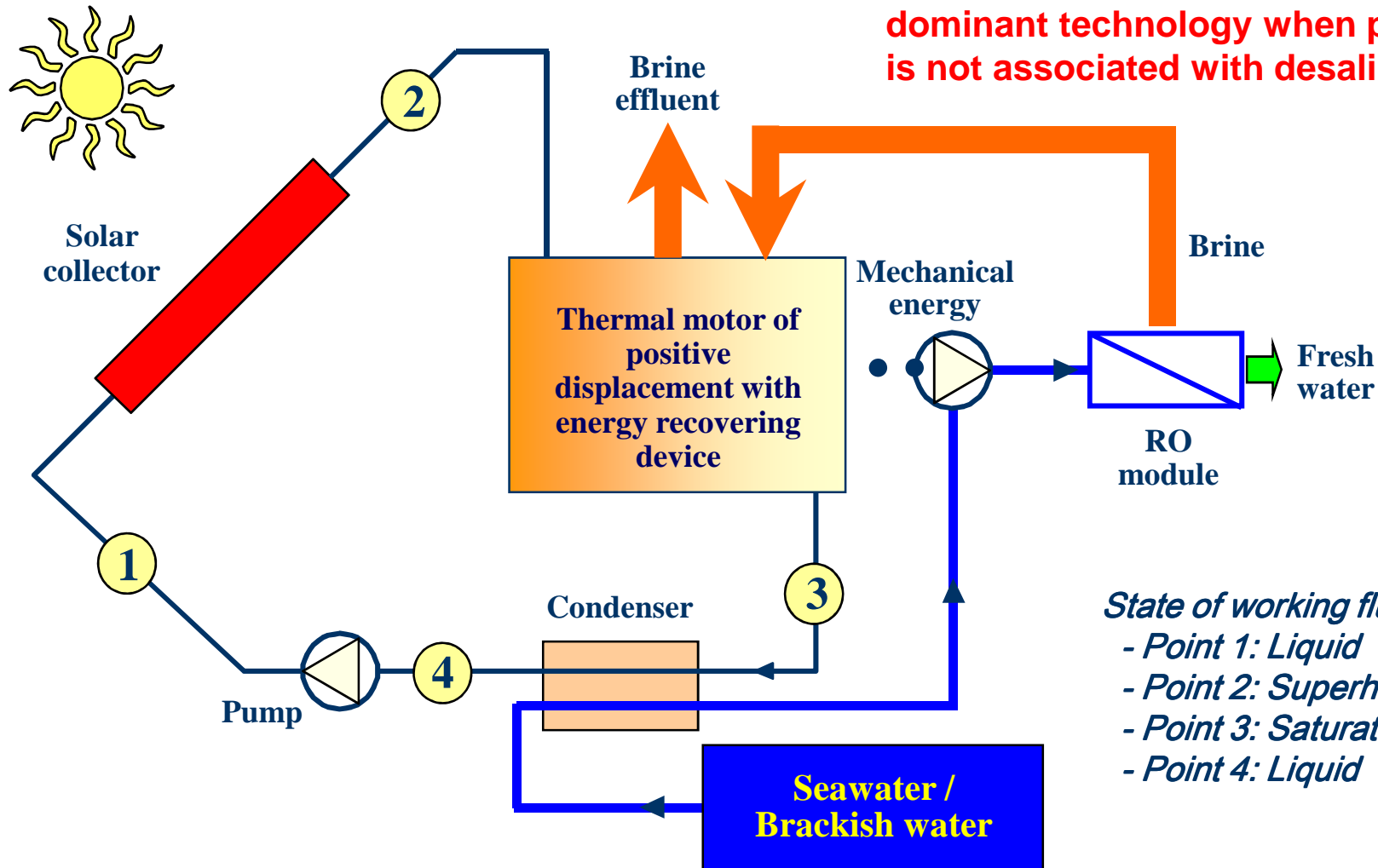
Membrane  
Distillation system  
installed at Prof. Dr.  
Hassan Fath facilities  
in Alexandria, Egypt  
(July 2005).

Fraunhofer Institut  
(Germany)



# THERMAL MOTOR + REVERSE OSMOSIS

Reverse Osmosis is the current dominant technology when power plant is not associated with desalination



*State of working fluid:*

- Point 1: Liquid
- Point 2: Superheated vapour
- Point 3: Saturated vapour
- Point 4: Liquid

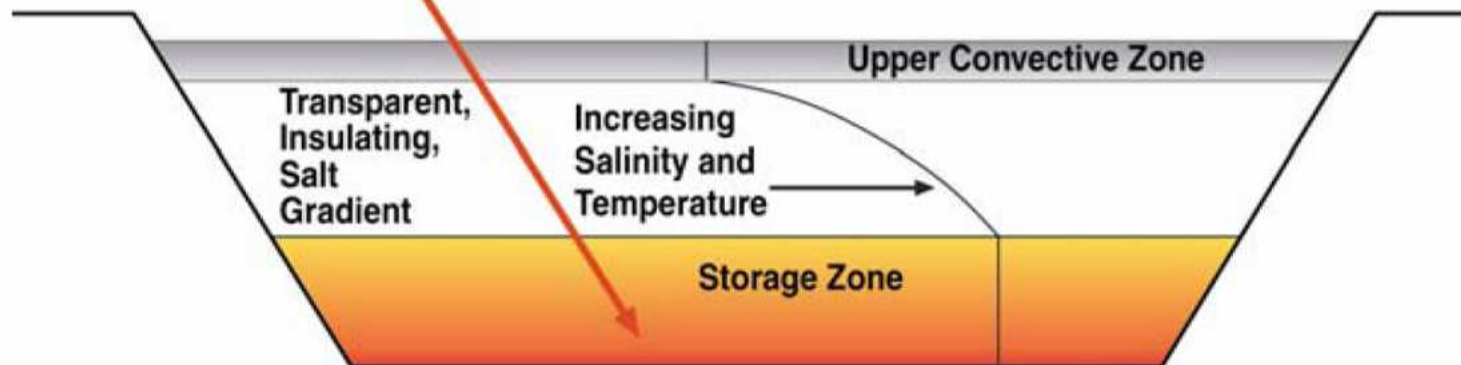


# SOLAR PONDS

## Long term storage of solar energy into a salt-gradient pond

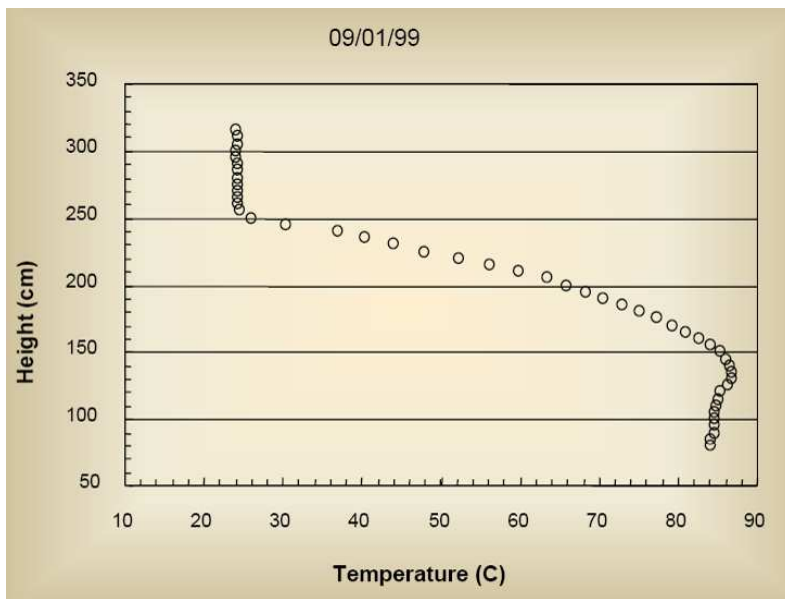


- Short solar waves are absorbed by water at the bottom
- The second layer acts as a thermal insulator.
- Average temperature 40-80°C

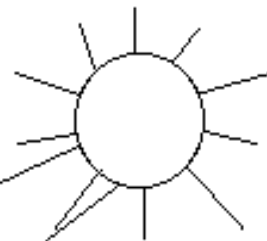




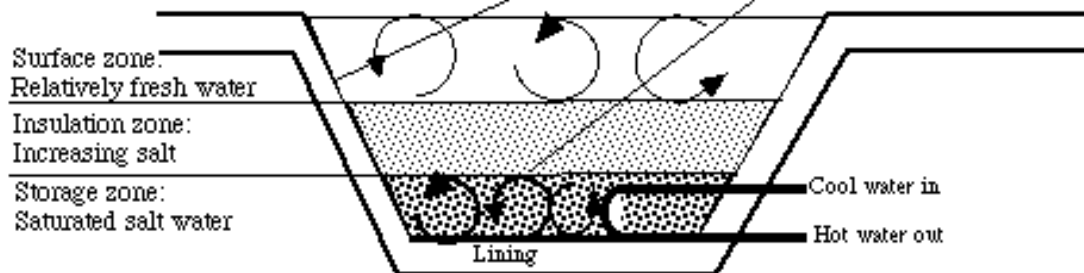
# SOLAR PONDS



Temperature distribution at Solar Pond of ENIT (Tunisia), 1500 m<sup>2</sup> and 3,5 m deep



Solar Pond of ENIT (Tunis)



# SOLAR PONDS



**Solar Ponds near Lisbon (Portugal) → 1024 m<sup>2</sup> with heat exchanger at the bottom**

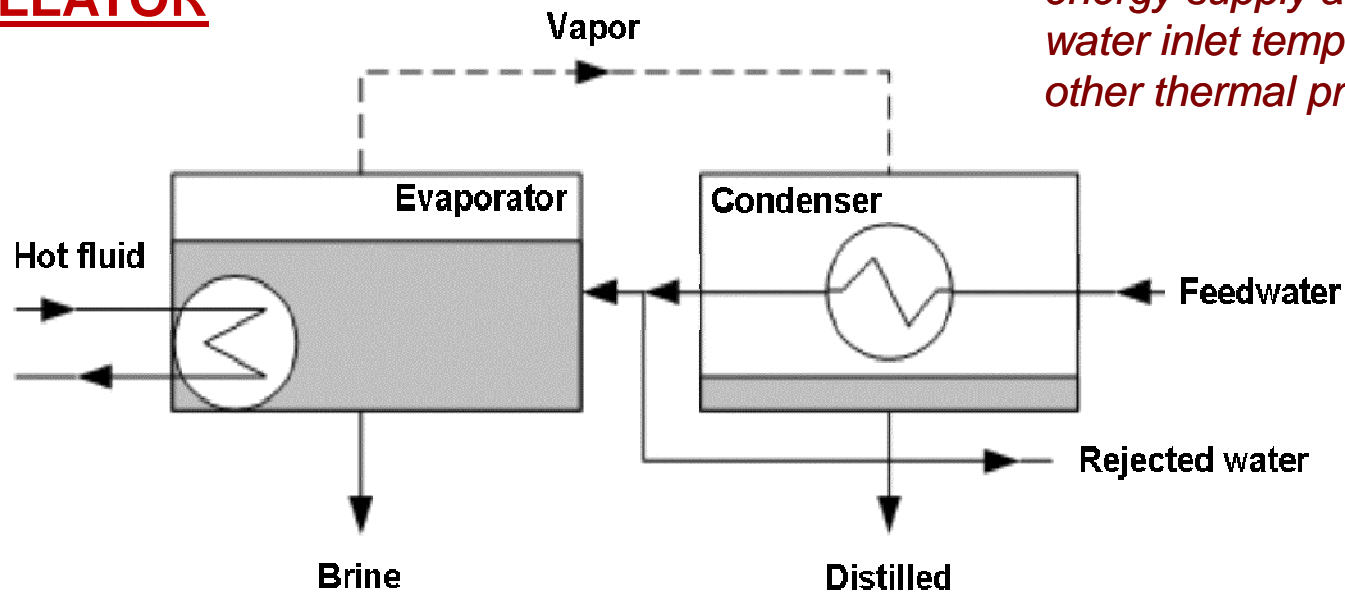


**Solar Ponds at El Paso (Texas)**  
→ one of 210,000 m<sup>2</sup> and another of 1,900,000 m<sup>2</sup>



# MULTI-EFFECT DISTILLATION (MED)

## ONE EFFECT DISTILLATOR



*MED process required lower energy supply and lower feed water inlet temperature than other thermal processes*



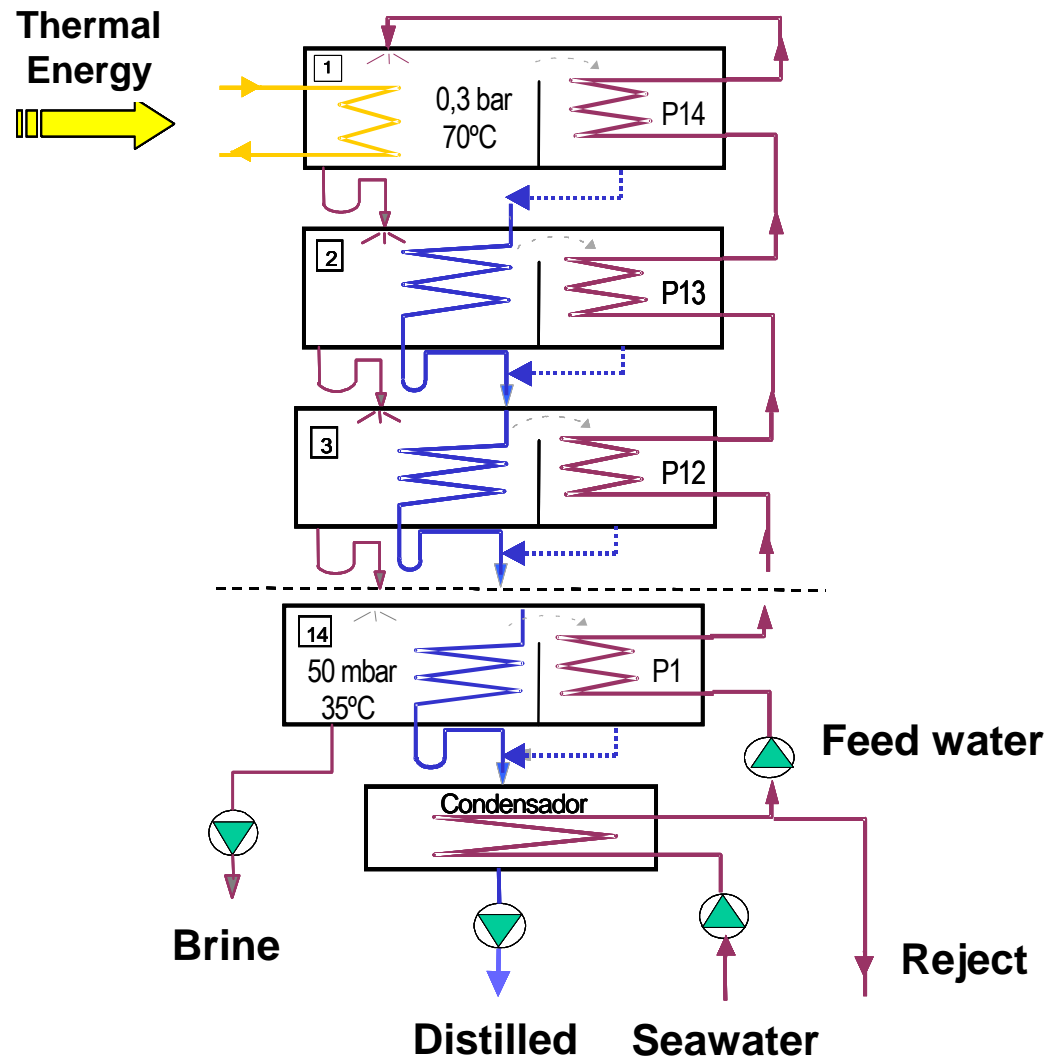
# MULTI-EFFECT DISTILLATION (MED)

The Performance Ratio is **higher** when the **number of effects is increased** (**MULTI-EFFECT DISTILLATION**)

because successive consecutive evaporations can be performed at decreasing temperatures, recovering the latent heat of evaporation.

Due to technical and economic reasons, MED commercial plans usually have between **4 and 8 effects**.

The distillation plant installed at the PSA is a forward-feed, vertically-stacked, multi-effect distillation unit with **14 effects**.



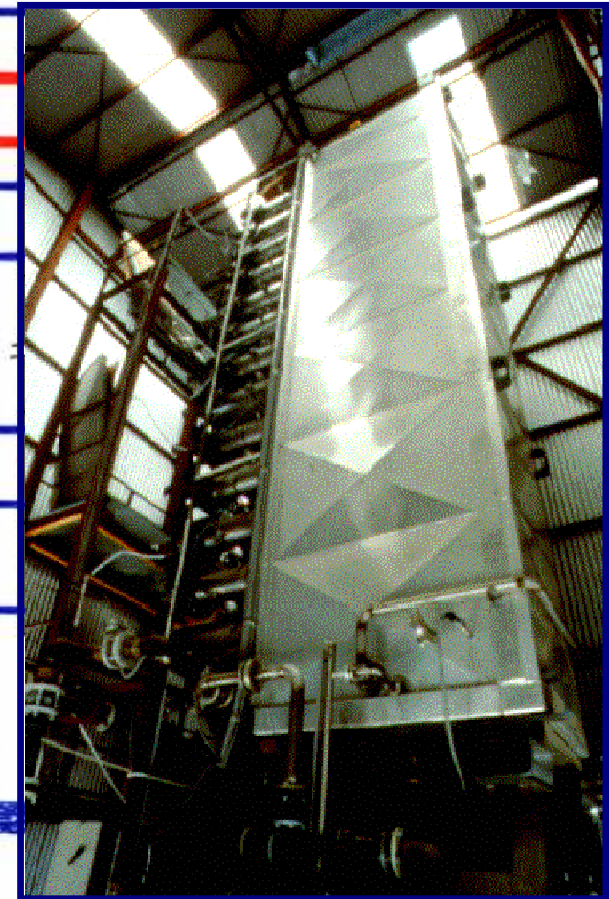
# MULTI-EFFECT DISTILLATION (MED)



**Conceptual scheme of  
MED plant coupled to solar  
collector field, developed  
at PSA during the 90's.  
Estimated water cost:  
1.80 – 2.20 €/m<sup>3</sup>**



**Final condenser  
seawater cooling  
(12 m<sup>3</sup>)**



**Brine  
(5 m<sup>3</sup>)**

**Seawater input  
(20 m<sup>3</sup>)**



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# AQUASOL PROJECT

Enhanced Zero Discharge Seawater Desalination using Hybrid Solar Technology (AQUASOL, FP5-EVK1-CT2001-00102) partially funded by the European Commission within the Energy, Environment and Sustainable Development Programme. Development of an environmentally-friendly improved cost- and energy efficient seawater desalination technology based on the multi-effect distillation process:

**14 effects MED plant (150 kW<sub>th</sub>, 2.5 m<sup>3</sup>/h distillate prod.)**

- ◆ **Stationary CPC solar collector field**
- ◆ **Thermal storage system (water, 24 m<sup>3</sup>)**
- ◆ **Double-effect (LiBr-H<sub>2</sub>O) absorption heat pump**
- ◆ **Smoke-tube gas boiler**
- ◆ **Solar dryer for final treatment of the brine**



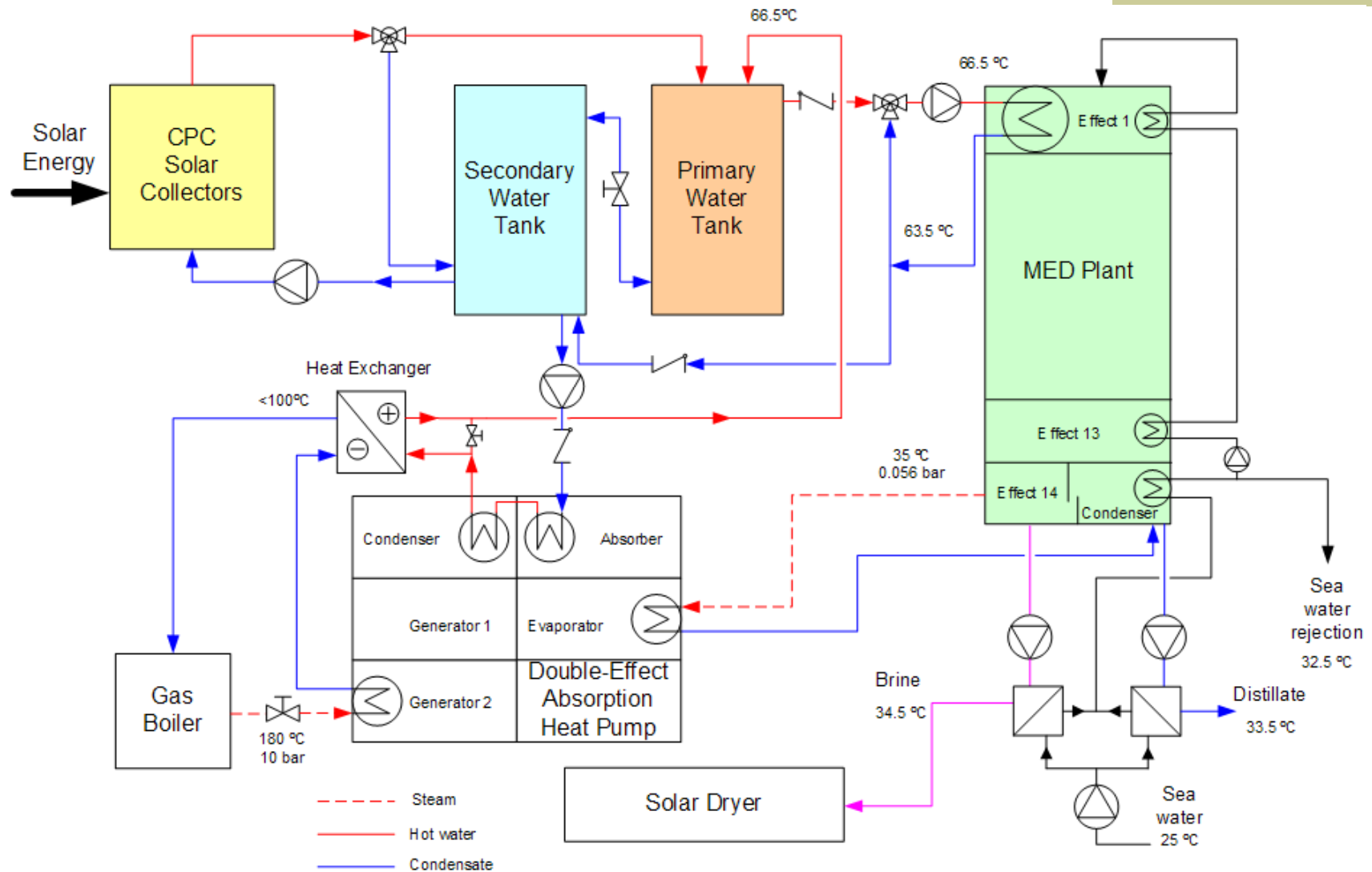
# AQUASOL OPERATING MODES

Three desalination system operating modes are possible depending on where the desalination unit energy supply comes from:

- **Solar-only mode**: energy to the first distillation effect comes exclusively from thermal energy from the solar collector field.
- **Fossil-only mode**: the double-effect heat pump supplies all of the heat required by the distillation plant.
- **Hybrid mode**: the energy comes from both the heat pump and the solar field. Two different operating philosophies are considered:
  - The heat pump works continuously 24 hours a day with a 30% minimum contribution.
  - Start-up and shutdown of the pump when requested, depending on the availability of the solar resource.

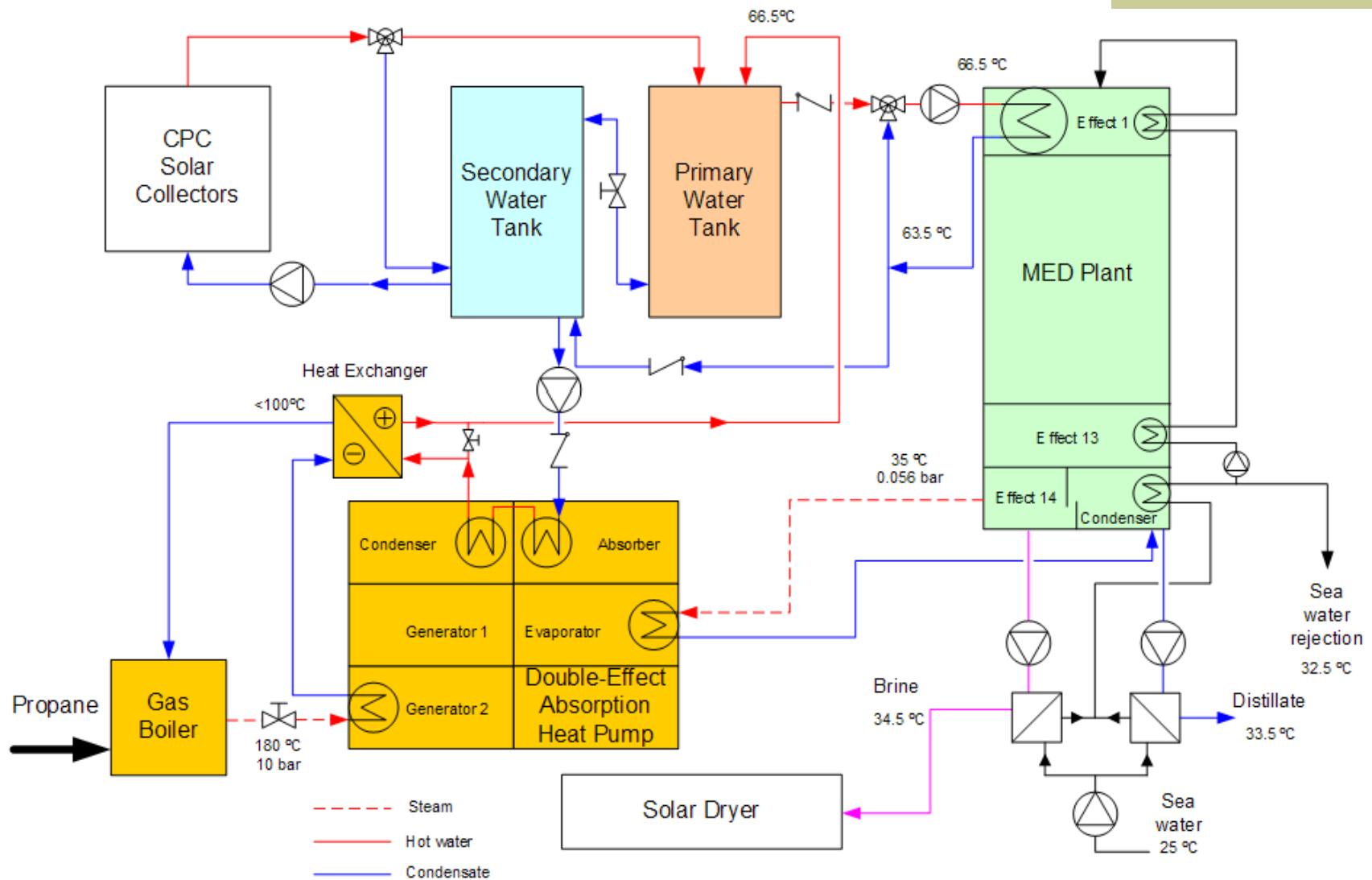


# AQUASOL OPERATION: SOLAR MODE

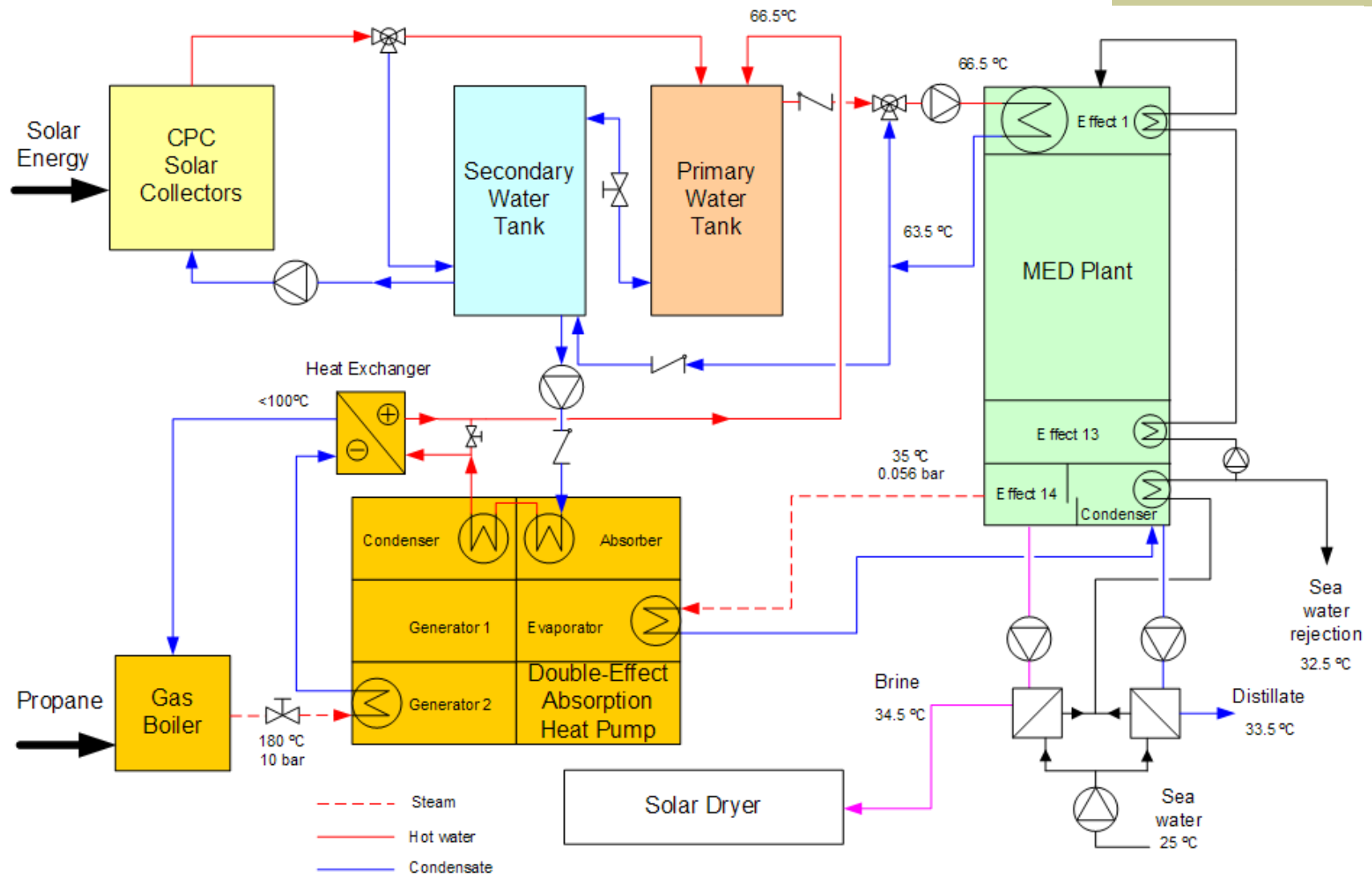




# AQUASOL OPERATION: FOSSIL MODE



# AQUASOL OPERATION: HYBRID MODE



# CPC SOLAR COLLECTOR FIELD

The solar field is made up of 252 stationary solar collectors (CPC Ao Sol 1.12x) with a total surface area of 500 m<sup>2</sup> arranged in four rows of 63 collectors.

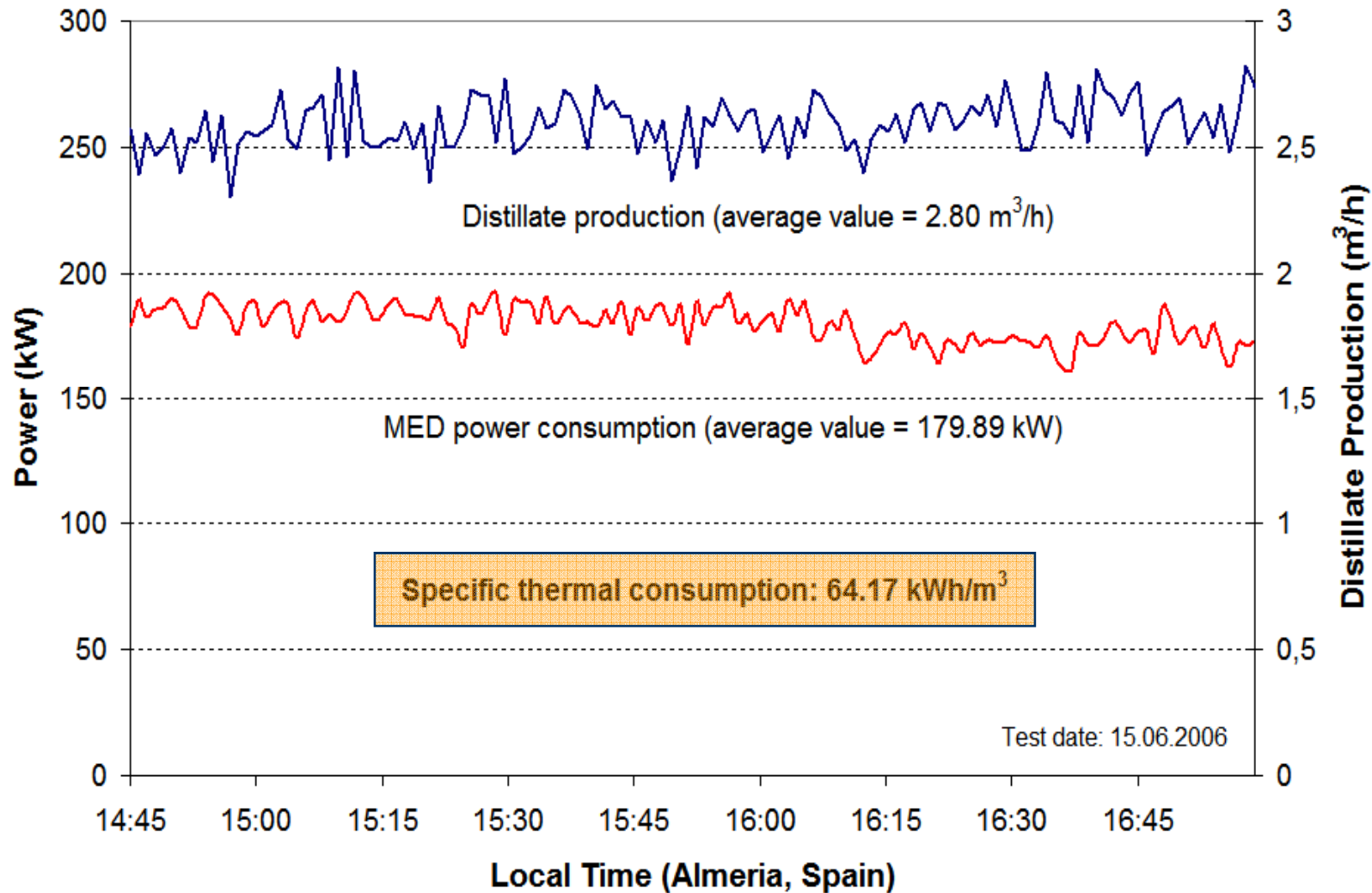


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# SOLAR-ONLY MODE



Distillate production and global thermal energy consumed by AQUASOL plant in **SOLAR-ONLY MODE**



# CONCLUSIONS & COST ESTIMATIONS

- Plant specific consumption of thermal energy, in the solar-only mode, is in the range of **60 to 70 kWh** per m<sup>3</sup> of distillate produced. These values are reduced to about 30 kWh per cubic meter when the absorption heat pump is working in fossil-only mode.
- The feasibility of a hybrid mode operation was demonstrated. The absorption machine presents a high thermal inertia but no problems have been detected during transients. However, further research in control should be done in order to keep the heat pump operation at maximum efficiency.
- AQUASOL production of 30 m<sup>3</sup> (from 09:00 to 21:00 h) → **60 L/m<sup>2</sup>** (winter day). Summer day: about **90 - 100 L/m<sup>2</sup>**. 1 Ha with a land occupation factor of 50% (5,000 m<sup>2</sup> of solar collectors) would yearly produce about a **160,000 m<sup>3</sup>**
- Cost of AQUASOL produced water: **8.12 €/m<sup>3</sup>** (PSA plant / 2.5 m<sup>3</sup>/h) → **0.93 €/m<sup>3</sup>** (extrapolation to a **12,000 m<sup>3</sup>/day** plant). Land cost not considered.
- Current environmental and energy scenarios makes unlikely that Solar Desalination will not play a major role in the coming years. It is reasonably expected that full industrial involvement would substantially reduce this cost.



# ACKNOWLEDGEMENTS

- Institute of Agronomy and Veterinary Hassan II
- EUROPEAN UNION
- CYCLER-SUPPORT PROJECT
- INNOVAMED PROJECT

**On-going projects at PSA about solar desalination**

- **POWERSOL. EC, FP6, 032344 (INCO)**
- **MEDESOL. EC, FP6, 036986 (GOCE)**
- **OSMOSOL. ENE2005-08381-C03.**

<http://www.psa.es/webeng/areas/quimica/proyectos.html>

